FLUID COOLING | Shell & Tube CA-2000 Series

COPPER & STEEL CONSTRUCTION

Features

- Super High Flow
- Largest Flow Rates & **Heat Transfer Available**
- ASME Code
- Rugged Steel Construction
- Custom Designs Available
- Competitively Priced
- 3/8" & 5/8" Tubes Available
- Max. 10" Diameter, 12' Long
- 150# ANSI/ASME Flanged Shell **Connections (Metric Available)**
- Optional Construction on CA-2000 Series: Tubes, Tubesheets, and End
- End Bonnets Removable For Servicing
- Saddle Brackets For Incremental Mounting
- ASME Code (Section VIII, Division I) and TEMA-C Construction Available (Consult Factory for Ordering Information)





Ratings

Maximum Shell Pressure 150 psi Maximum Tube Side Pressure 150 psi Maximum Temperature 300° F

Materials

Headers Steel

Shell Steel

Shell Connections Steel

Baffles Brass

End Bonnets Cast Iron

Mounting Brackets Steel/Cast Iron

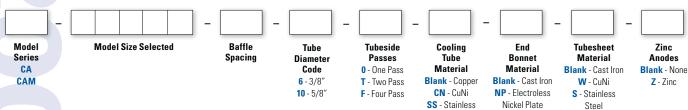
Gaskets Nitrile Rubber/Cellulose Fiber

Nameplate Aluminum Foil

Maximum Flow Rates

| Shell Side (GPM) | | Tube Side GPM | | | |
|------------------|--------------|---------------|-------------|--------------|--|
| 6" Baffle | 9″ Baffle | One Pass | Two Pass | Four Pass | |
| 210 | 320 | 652 | 326 | 163 | |

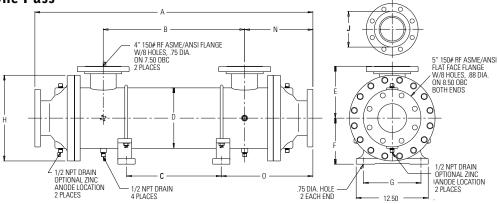
How to Order



CA = NPT tubeside bottom connections; ASME/ANSI flange shell top connections. **CAM** = BSPP shellside connections; BSPP tubeside connections.

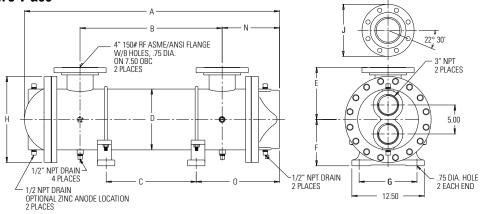
Dimensions





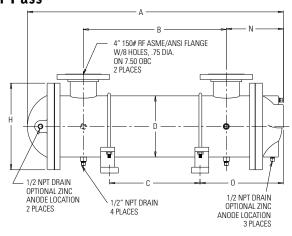
| Model | Α | N | 0 |
|----------|--------|-------|-------|
| CA-2036 | 49.64 | | |
| CA-2048 | 61.64 | | |
| CA-2060 | 73.64 | | |
| CA-2072 | 85.64 | | |
| CA-2084 | 97.64 | 11.82 | 15.92 |
| CA-2096 | 109.64 | | |
| CA-20108 | 121.64 | | |
| CA-20120 | 133.64 | | |
| CA-20132 | 145.64 | | |
| CA-20144 | 157.64 | | |

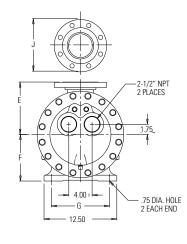
Two Pass



| Model | A | N | 0 |
|----------|--------|------|-------|
| CA-2036 | 45.55 | | |
| CA-2048 | 57.55 | | |
| CA-2060 | 69.55 | | |
| CA-2072 | 81.55 | | |
| CA-2084 | 93.55 | 9.90 | 14.38 |
| CA-2096 | 105.55 | | |
| CA-20108 | 117.55 | | |
| CA-20120 | 129.55 | | |
| CA-20132 | 141.55 | | |
| CA-20144 | 153.55 | | |
| | | | |

Four Pass





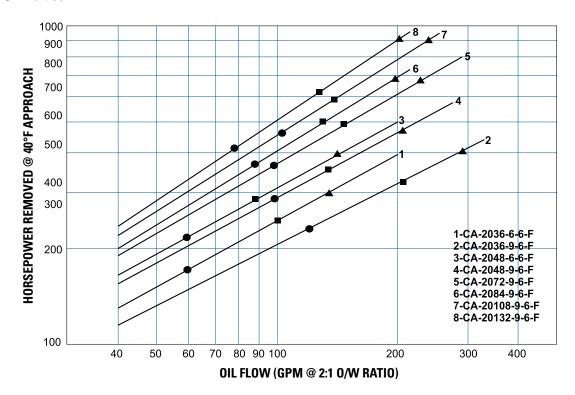
| Model | В | С | D | Е | F | G | Н | J |
|----------|-----|-----|----------|---|---|----|-----------|----------|
| CA-2036 | 26 | 18 | | | | | | |
| CA-2048 | 38 | 30 | | | | | | |
| CA-2060 | 50 | 42 | | | | | | 6.19 DIA |
| CA-2072 | 62 | 54 | | | | | | Raised |
| CA-2084 | 74 | 66 | 10.5 DIA | 9 | 8 | 10 | 14.88 DIA | Face |
| CA-2096 | 86 | 78 | | | | | | 2 Places |
| CA-20108 | 98 | 90 | | | | | | |
| CA-20120 | 110 | 102 | | | | | | |
| CA-20132 | 122 | 114 | | | | | | |
| CA-20144 | 134 | 126 | | | | | | |

| Model | A | N | 0 |
|----------|--------|------|-------|
| CA-2036 | 45.34 | | |
| CA-2048 | 57.34 | | |
| CA-2060 | 69.34 | | |
| CA-2072 | 81.34 | | |
| CA-2084 | 93.34 | 9.78 | 13.78 |
| CA-2096 | 105.34 | | |
| CA-20108 | 117.34 | | |
| CA-20120 | 129.34 | | |
| CA-20132 | 141.34 | | |
| CA-20144 | 153.34 | | |
| | | | |

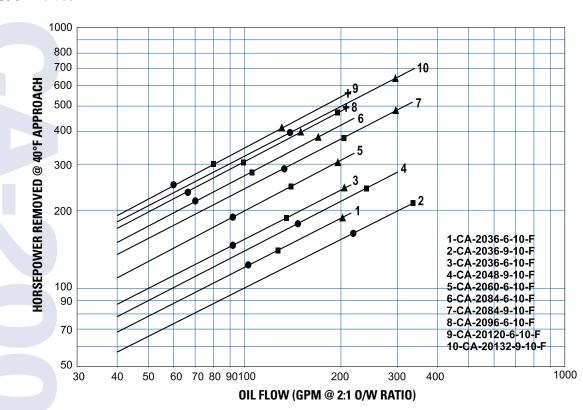
NOTE: We reserve the right to make reasonable design changes without notice. Dimensions are in inches.

Performance Curves

3/8" **Tubes**



5/8" Tubes



Selection Procedure

Performance Curves are based on 100SSU oil leaving the cooler 40°F higher than the incoming water temperature (40°F approach temperature). Curves are based on a 2:1 oil to water ratio.

Step 1

Determine the Heat Load. This will vary with different systems, but typically coolers are sized to remove 25 to 50% of the input nameplate horsepower. (Example: 100 HP Power Unit x .33 = 33 HP Heat load.)

If BTII/Hr is known: HP = BTU/Hr

If BTU/Hr. is known: HP = $\frac{BTU/H}{2545}$

Step 2

 $\label{lem:decomposition} \textbf{Determine Approach Temperature}.$

Desired oil leaving cooler °F — Water Inlet temp. °F = Actual Approach

Step 3

Determine Curve Horsepower Heat Load. Enter the

information from above:

HP heat load x $\frac{40}{\text{Actual Approach}}$ x $\frac{\text{Viscosity}}{\text{Correction A}} = \frac{\text{Curve}}{\text{Horsepower}}$

Step 4

Enter curves at oil flow through cooler and curve horsepower. Any curve above the intersecting point will work.

Step 5

Determine Oil Pressure Drop from Curves. Multiply pressure drop from curve by correction factor B found on oil viscosity correction curve.

 \bullet = 5 PSI; \blacksquare = 10 PSI; \blacktriangle = 20 PSI; 昔 = 40 PSI.

Oil Temperature

Oil coolers can be selected by using entering or leaving oil tempertures.

Typical operating temperature ranges are:

Hydraulic Motor Oil 110°F - 130°F Hydrostatic Drive Oil 130°F - 180°F Lube Oil Circuits 110°F - 130°F Automatic Transmission Fluid 200°F - 300°F

Desired Reservoir Temperature

Return Line Cooling: Desired temperature is the oil temperature leaving the cooler. This will be the same temperature that will be found in the reservoir.

Off-Line Recirculation Cooling Loop: Desired temperature is the temperature entering the cooler. In this case, the oil temperature change must be determined so that the actual oil leaving temperature can be found. Calculate the oil temperature change (Oil \triangle T) with this formula:

Oil $\triangle T = (BTU's/Hr.)/GPM$ Oil Flow x 210).

To calculate the oil leaving temperature from the cooler, use this formula:

Oil Leaving Temperature = Oil Entering Temperature - Oil $\triangle T$.

This formula may also be used in any application where the only temperature available is the entering oil temperature.

Oil Pressure Drop: Most systems can tolerate a pressure drop through the heat exchanger of 20 to 30 PSI. Excessive pressure drop should be avoided. Care should be taken to limit pressure drop to 5 PSI or less for case drain applications where high back pressure may damage the pump shaft seals.

